

Boise State University

ScholarWorks

---

Mathematics Faculty Publications and  
Presentations

Department of Mathematics

---

9-10-2008

## A Parallel Computational Method for Simulating Two-Phase Gel Dynamics

Jian Du

*University of Utah*

Aaron L. Fogelson

*University of Utah*

Grady Wright

*Boise State University*

---

This is an author-produced, peer-reviewed version of this article. The final, definitive version of this document can be found online at *International Journal for Numerical Methods in Fluids*, published by Institution of Engineering and Technology. Copyright restrictions may apply. DOI: [10.1002/flid.1907](https://doi.org/10.1002/flid.1907)

# A parallel computational method for simulating two-phase gel dynamics

Jian Du<sup>1 † \*</sup>, Aaron L. Fogelson<sup>1,2</sup> and Grady B. Wright<sup>3</sup>

<sup>1</sup> *Department of Mathematics, University of Utah,  
Salt Lake City, UT 84112-0090, USA*

<sup>2</sup> *Department of Bioengineering, University of Utah,  
Salt Lake City, UT 84112-0090, USA*

<sup>3</sup> *Department of Mathematics, Boise State University,  
Boise, ID 83725-1555, USA*

## SUMMARY

We develop a parallel computational algorithm for simulating models of gel dynamics where the gel is described by two phases, a networked polymer and a fluid solvent. The models consist of transport equations for the two phases, two coupled momentum equations, and a volume-averaged incompressibility constraint. Multigrid with Vanka-type box relaxation scheme is used as preconditioner for the Krylov subspace solver (GMRES) to solve the momentum and incompressibility equations. Through numerical experiments of a model problem, the efficiency, robustness and scalability of the algorithm are illustrated. Copyright © 2000 John Wiley & Sons, Ltd.

KEY WORDS: multiphase flow; multigrid; Vanka relaxation; GMRES; preconditioning

## 1. INTRODUCTION

Polymer gels are composed of two materials: a polymer network and a solvent. By weight and volume gels are mostly solvent, but the rheology of the gel can range from a very viscous fluid to an elastic solid. In addition to viscoelastic stresses, gels can exhibit chemical stresses which result in swelling and deswelling behavior.

A commonly used model for the mechanics of gels is the two-phase flow (or two-fluid) model [1, 2, 3, 4, 5, 6, 7]. Each phase, network and solvent, is treated as a continuum and moves according to its own velocity field. Each region in space is composed of a mixture of the two phases that is described by the volume fractions of the phases. The equations of motion for the gel consist of two coupled momentum equations and two continuity equations. These models of gels are based on mixture theory [8, 9], which has been used for many applications and is becoming increasingly popular in models of biological materials such as tissue [10],

---

\*Correspondence to: 155 South 1400 East Room 233, Salt Lake City, UT 84112-0090, USA

†Email: du@math.utah.edu

tumors [11, 12], cytoplasm [1, 3, 4, 6], and biofilms [13, 14, 2]. While much work has gone into advancing these models, the same is not true for the development of efficient numerical methods for simulating them. Since repeated simulation of models is crucial for validating their usefulness, the need for fast and robust computational methods is essential. A significant step in this direction was described in [15] where a novel serial algorithm for a subdivision of the problems was introduced.

In this paper we extend the work in [15] by proposing a parallel computational methodology for solving the same problems. Both the network and solvent are modeled as viscous fluids. The viscosity of the network is much larger than that of the solvent. The gel feels a chemical pressure that makes the system bistable, that is, it drives the network volume fraction to one of two preferred states. Under appropriate conditions the chemical pressure induces phase separation of the mixture and is a good test for the robustness of any numerical procedure. Computational tests of the proposed method are carried out for the model in two dimensions, from which the efficiency and robustness of the algorithm are investigated.

In many models of gel dynamics, including our model problem, viscous terms are assumed to dominate so that inertial terms are negligible. This assumption leads to an elliptic system for the coupled momentum and incompressibility equations that resembles Stokes equations. However, there are many key differences which increase the complexity of the problem. First, since there are two phases, there are two sets of momentum equations. Second, there are off-diagonal terms coupling the two velocity fields (and the components of the two fields) together. Third, the Laplacians involve time-dependent variable coefficients related to the volume fractions of the two phases. Finally, incompressibility is replaced with a “volume averaged” incompressibility over the two fluids.

We use second-order finite-differences on a marker-and-cell (MAC) grid [16] to discretize this system. As with Stokes (and linearized Navier-Stokes) equations, this gives rise to a large, sparse linear system of saddle point type. In [15], we developed an extension of a multigrid method initially proposed for Stokes and Navier-Stokes equations by Vanka [17], and which has seen considerable development in the past several years (see, for example, [18, 19, 20, 21, 22, 23]). The method is characterized by the smoother used and is referred to in literature as box [22, pp. 320-322], coupled [23], or Vanka [19] relaxation. The basic idea of the smoother is to compute updates to the solution by collectively solving for the velocity and pressure in the discrete momentum equations locally, computational cell (or box) by cell. For the gel system, this means solving a  $(2^{d+1} + 1)$ -by- $(2^{d+1} + 1)$  saddle point system for each cell, where  $d$  is the number of spatial dimensions. Depending on how the cells are processed (Jacobi or Gauss-Seidel like), the method can also be viewed as an additive or multiplicative Schwarz domain decomposition method, where the subdomains consist of a single computational cell [19]. We use the smoother with standard prolongation and restriction operators and do a direct discretization of the equations on the coarse grids, which makes the implementation relatively simple.

When the network and solvent are well mixed, the multigrid box-relaxation method performs quite well as a solver for the model problem considered here. However, as phase separation occurs, the solver performance degrades quite dramatically, and it, in fact, fails in some cases as shown in [15]. One particularly effective way of improving the robustness of a non-optimal (or even non-converging) multigrid method is to combine it with a Krylov subspace method (see, for example, [22, §7.8]). In the current paper, a parallel version of the algorithm in [15] is developed which combines the Krylov subspace solver in PETSc [24] with the multigrid

box-relaxation scheme as the preconditioner.

In addition to the momentum and incompressibility equations, models for gel dynamics include equations for the transport of the network and solvent. For the transport equations we use a conservative finite-volume discretization in which the advection term is treated explicitly with first-order upwinding and the diffusion term is handled implicitly with backward Euler.

The rest of the paper is organized as follows. In Section 2, the model problem for describing and testing the computational method is introduced. Section 3 describes the discretization (in space and time) for the 2-D model. In Section 4, the elements of the multigrid box-relaxation scheme are introduced with parallel considerations, followed by a description of its role as a preconditioner for GMRES (generalized minimum residual). Section 5 presents the results of simulations as well as the parallel performance.

## 2. MODEL PROBLEM

The model problem we consider is for a gel composed of two immiscible materials, a polymer network and a fluid solvent. We assume that the total amount of gel remains constant and that the transport of the network and solvent is governed by the equations:

$$\frac{\partial \theta^n}{\partial t} + \nabla \cdot (\theta^n \mathbf{u}^n) = 0 \quad (1)$$

$$\frac{\partial \theta^s}{\partial t} + \nabla \cdot (\theta^s \mathbf{u}^s) = 0 \quad (2)$$

where  $\theta^n$ , and  $\theta^s = 1 - \theta^n$  are the respective volume fractions of the network and solvent,  $0 < \theta^n < 1$ , and  $\mathbf{u}^n$  and  $\mathbf{u}^s$  are the respective transport velocities. Adding these two equations, and using  $\theta^n + \theta^s = 1$  gives the incompressibility-type constraint

$$\nabla \cdot (\theta^n \mathbf{u}^n + \theta^s \mathbf{u}^s) = 0 \quad (3)$$

The transport velocities are determined by conservation of momentum. We assume the network acts as a constant density viscous material and the solvent acts as a Newtonian fluid of much less viscosity. Viscous terms are assumed to dominate so that inertial terms are negligible (similar to zero-Reynolds number flow), i.e. the system responds instantaneously to applied forces.

The network and solvent are each subject to a number of intraphase stresses. We assume that the viscous stress tensors  $\underline{\underline{\sigma}}^n$  and  $\underline{\underline{\sigma}}^s$  for the network and solvent are proportional to the respective gradient of the network and solvent velocities, i.e.

$$\underline{\underline{\sigma}}^n = \mu_n \left( \nabla \mathbf{u}^n + \nabla \mathbf{u}^{nT} \right) + \lambda_n \delta_{ij} \nabla \cdot \mathbf{u}^n \quad (4)$$

$$\underline{\underline{\sigma}}^s = \mu_s \left( \nabla \mathbf{u}^s + \nabla \mathbf{u}^{sT} \right) + \lambda_s \delta_{ij} \nabla \cdot \mathbf{u}^s \quad (5)$$

where  $\mu_{n,s}$  are shear viscosities and  $\lambda_{n,s} + 2\mu_{n,s}/d$  are the bulk viscosities of the network and solvent ( $d$  is the dimension). The network and solvent are also subject to a frictional drag since the motion of the solvent influences the network. We model this by  $\beta \theta^n \theta^s (\mathbf{u}^n - \mathbf{u}^s)$ , where  $\beta > 0$  is the drag coefficient. The third force on each phase is due to hydrostatic pressure. Since the polymer is assumed to be chemically active within the gel and the solvent is assumed to be

chemically neutral, the final force is generated by a chemical pressure,  $\Psi(\theta^n)$ , and acts only on the network. The form of  $\Psi(\theta^n)$  used in this paper is described below.

Balancing the above forces on the network and solvent yields the equations:

$$\nabla \cdot (\theta^n \underline{\underline{\sigma}}^n) - \beta \theta^n \theta^s (\mathbf{u}^n - \mathbf{u}^s) - \theta^n \nabla p = \nabla \Psi(\theta^n) \quad (6)$$

$$\nabla \cdot (\theta^s \underline{\underline{\sigma}}^s) - \beta \theta^n \theta^s (\mathbf{u}^s - \mathbf{u}^n) - \theta^s \nabla p = 0 \quad (7)$$

where  $p$  is the hydrostatic pressure. These two equations, combined with (1) and (3), and subject to suitable boundary conditions, govern the gel dynamics and are the same as used in [1, 3, 4, 6, 15]. For our test problem we assume no-slip boundary conditions for the network and solvent velocities, and no-flux boundary conditions for  $\theta^n$  and  $\theta^s$ .

The chemical pressure includes osmotic pressure, but it may also include active, contractile stresses such as in the actomyosin gels of cytoplasm. In this paper we are not concerned with the origins of the chemical stress, and refer to it simply as the osmotic pressure. We assume the osmotic pressure is of the form

$$\Psi(\theta^n) = \gamma \theta^n (\theta^n - \theta_0^n) (\theta^n - \theta_*^n) \quad (8)$$

where  $\gamma > 0$ ,  $0 < \theta_0^n < \theta_*^n < 1$ ; see Figure 1 for a plot of  $\Psi(\theta^n)$  with parameters used in the numerical experiments that follow. This functional form is chosen since it can produce phase separation, or channeling. In regions of space where  $\Psi'(\theta^n) > 0$  the mixture is stable, but where  $\Psi'(\theta^n) < 0$  the mixture tends to phase separate; see Cogan and Keener [2] for an analysis. This form of  $\Psi$  does not allow the phases to separate completely. Phase separation is generally observed in gels [7], and is vital for locomotion and for transporting nutrients in some amoeboid cells [25].

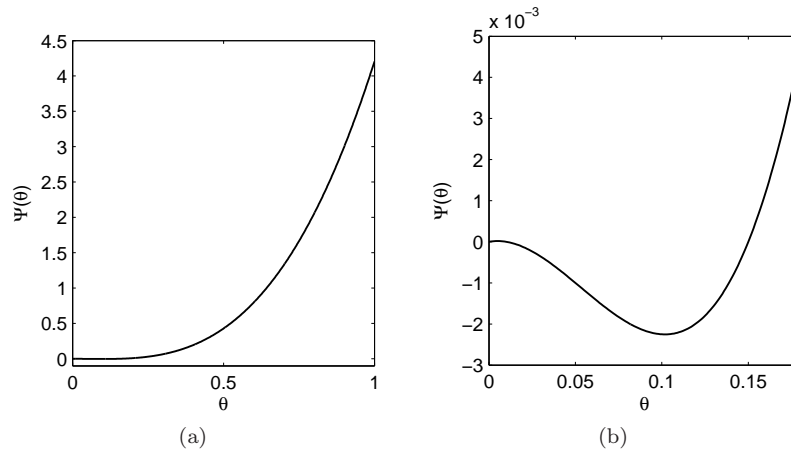


Figure 1: (a) Osmotic pressure function (8) from the model problem with parameters  $\gamma = 5$ ,  $\theta_0^n = 0.01$  and  $\theta_*^n = 0.15$  used in the numerical experiments. (b) A detailed plot of this function near the origin.

Finally, we assume there is a small amount of diffusion between the network and solvent in the gel. This is mathematically and computationally useful since it means the transition

between the network and solvent will be smooth even in areas where the two phases have separated. This additional assumption changes (1) and (2) to

$$\frac{\partial \theta^n}{\partial t} + \nabla \cdot (\theta^n \mathbf{u}^n) = \kappa \nabla^2 \theta^n \quad (9)$$

$$\frac{\partial \theta^s}{\partial t} + \nabla \cdot (\theta^s \mathbf{u}^s) = \kappa \nabla^2 \theta^s \quad (10)$$

where  $\kappa \geq 0$  is the diffusion constant. We use relatively small diffusion coefficients so that this modification does not change the qualitative features of the model, but ensures the solution is continuous.

### 3. DISCRETIZATION

Let  $\mathbf{u}^n = (u^n, v^n)^T$  and  $\mathbf{u}^s = (u^s, v^s)^T$ , where  $u^n, v^n$  and  $u^s, v^s$  are the respective network and solvent velocity components in the  $x$  and  $y$  directions, and let the spatial domain be  $\Omega = \{(x, y) | 0 \leq x \leq a, 0 \leq y \leq b\}$ . Then the momentum equations (6)–(7) and volume-averaged incompressibility (3) are given in matrix-vector form as

$$\begin{bmatrix} \mathcal{L}_n - \mathcal{C} & \mathcal{C} & -\mathcal{G}_n \\ \mathcal{C} & \mathcal{L}_s - \mathcal{C} & -\mathcal{G}_s \\ -\mathcal{D}_n^T & -\mathcal{D}_s^T & 0 \end{bmatrix} \begin{bmatrix} \mathbf{u}^n \\ \mathbf{u}^s \\ p \end{bmatrix} = \begin{bmatrix} \nabla \Psi(\theta^n) \\ 0 \\ 0 \end{bmatrix} \quad (11)$$

where

$$\begin{aligned} \mathcal{L}_{n,s} &= \begin{bmatrix} \alpha_{n,s} \partial_x (\theta^{n,s} \partial_x) + \mu_{n,s} \partial_y (\theta^{n,s} \partial_y) & \mu_{n,s} \partial_y (\theta^{n,s} \partial_x) + \lambda_{n,s} \partial_x (\theta^{n,s} \partial_y) \\ \mu_{n,s} \partial_x (\theta^{n,s} \partial_y) + \lambda_{n,s} \partial_y (\theta^{n,s} \partial_x) & \alpha_{n,s} \partial_x (\theta^{n,s} \partial_x) + \mu_{n,s} \partial_y (\theta^{n,s} \partial_y) \end{bmatrix} \\ \mathcal{C} &= \begin{bmatrix} \beta \theta^n \theta^s & 0 \\ 0 & \beta \theta^n \theta^s \end{bmatrix}, \quad \mathcal{G}_{n,s} = \begin{bmatrix} \theta^{n,s} \partial_x \\ \theta^{n,s} \partial_y \end{bmatrix}, \quad \mathcal{D}_{n,s} = \begin{bmatrix} \partial_x \theta^{n,s} \\ \partial_y \theta^{n,s} \end{bmatrix} \end{aligned}$$

and  $\alpha_{n,s} = (2\mu_{n,s} + \lambda_{n,s})$ . Since  $\theta^s = 1 - \theta^n$ , we need only an equation for the transport of  $\theta^n$ , which is again given by (9). We use no-slip boundary conditions for (11) and no-flux for (9). Finally, the cubic function (8) is used for modeling the osmotic pressure.

For the spatial discretization we use a MAC grid where the positions of the unknowns are indicated in Figure 2. The mesh-spacing in the  $x$  and  $y$  direction is set equal and is given by  $h$ .

All equations in (11) are discretized using second-order, centered finite differences, which leads to the following approximation of the first row of (11) at the interior point  $(x_{i+\frac{1}{2},j}, y_{i+\frac{1}{2},j})$ :

$$\begin{aligned} & \frac{\alpha_n}{h^2} \left[ \theta_{i+1,j}^n (u_{i+\frac{3}{2},j}^n - u_{i+\frac{1}{2},j}^n) - \theta_{i,j}^n (u_{i+\frac{1}{2},j}^n - u_{i-\frac{1}{2},j}^n) \right] + \\ & \frac{\mu_n}{h^2} \left[ \bar{\theta}_{i+\frac{1}{2},j+\frac{1}{2}}^n (u_{i+\frac{1}{2},j+1}^n - u_{i+\frac{1}{2},j}^n) - \bar{\theta}_{i+\frac{1}{2},j-\frac{1}{2}}^n (u_{i+\frac{1}{2},j}^n - u_{i+\frac{1}{2},j-1}^n) \right] + \\ & \frac{\mu_n}{h^2} \left[ \bar{\theta}_{i+\frac{1}{2},j+\frac{1}{2}}^n (v_{i+1,j+\frac{1}{2}}^n - v_{i,j+\frac{1}{2}}^n) - \bar{\theta}_{i+\frac{1}{2},j-\frac{1}{2}}^n (v_{i+1,j-\frac{1}{2}}^n - v_{i,j-\frac{1}{2}}^n) \right] + \\ & \frac{\lambda_n}{h^2} \left[ \theta_{i+1,j}^n (v_{i+1,j+\frac{1}{2}}^n - v_{i+1,j-\frac{1}{2}}^n) - \theta_{i,j}^n (v_{i,j+\frac{1}{2}}^n - v_{i,j-\frac{1}{2}}^n) \right] - \\ & \beta \bar{\theta}_{i+\frac{1}{2},j}^n \bar{\theta}_{i+\frac{1}{2},j}^s (u_{i+\frac{1}{2},j}^n - u_{i+\frac{1}{2},j}^s) - \bar{\theta}_{i+\frac{1}{2},j}^n \frac{p_{i+1,j} - p_{i,j}}{h} = \frac{\Psi(\theta_{i+1,j}^n) - \Psi(\theta_{i,j}^n)}{h} \end{aligned} \quad (12)$$

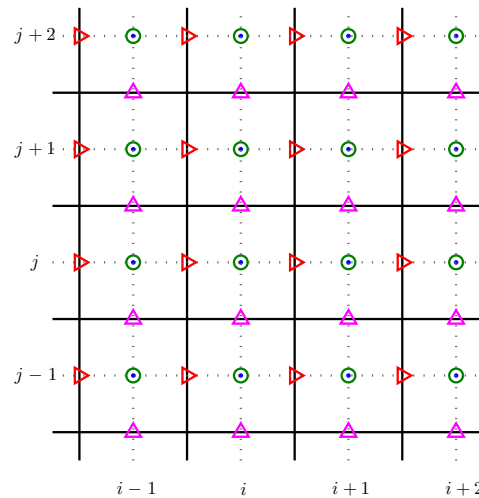


Figure 2: Location of the unknowns in the MAC grid for the 2-D gel model: ▷=network/solvent horizontal velocity, △=network/solvent vertical velocity, ● =pressure, and ○ =network/solvent volume fractions.

while the approximation to the second row at the interior point  $(x_{i,j+\frac{1}{2}}, y_{i,j+\frac{1}{2}})$  is given by:

$$\begin{aligned}
 & \frac{\mu_n}{h^2} \left[ \bar{\theta}_{i+\frac{1}{2},j+\frac{1}{2}}^n (u_{i+\frac{1}{2},j+1}^n - u_{i+\frac{1}{2},j}^n) - \bar{\theta}_{i-\frac{1}{2},j+\frac{1}{2}}^n (u_{i-\frac{1}{2},j+1}^n - u_{i-\frac{1}{2},j}^n) \right] + \\
 & \frac{\lambda_n}{h^2} \left[ \theta_{i,j+1}^n (u_{i+\frac{1}{2},j+1}^n - u_{i-\frac{1}{2},j+1}^n) - \theta_{i,j}^n (u_{i+\frac{1}{2},j}^n - u_{i-\frac{1}{2},j}^n) \right] + \\
 & \frac{\alpha_n}{h^2} \left[ \theta_{i,j+1}^n (v_{i,j+\frac{3}{2}}^n - v_{i,j+\frac{1}{2}}^n) - \theta_{i,j}^n (v_{i,j+\frac{1}{2}}^n - v_{i,j-\frac{1}{2}}^n) \right] + \\
 & \frac{\mu_n}{h^2} \left[ \bar{\theta}_{i+\frac{1}{2},j+\frac{1}{2}}^n (v_{i+1,j+\frac{1}{2}}^n - v_{i,j+\frac{1}{2}}^n) - \bar{\theta}_{i-\frac{1}{2},j+\frac{1}{2}}^n (v_{i,j+\frac{1}{2}}^n - v_{i-1,j+\frac{1}{2}}^n) \right] - \\
 & \beta \bar{\theta}_{i,j+\frac{1}{2}}^n \bar{\theta}_{i,j+\frac{1}{2}}^s (v_{i,j+\frac{1}{2}}^n - v_{i,j+\frac{1}{2}}^s) - \bar{\theta}_{i,j+\frac{1}{2}}^n \frac{p_{i,j+1} - p_{i,j}}{h} = 0
 \end{aligned} \tag{13}$$

Bars over  $\theta^n$  and  $\theta^s$  represent arithmetic averages of the values of these variables at nearest neighbor cells with two-point averages when there is a mix of integer and half-integer indices, and four-point averages when there are two half-integer indices. The discretizations of the third and fourth row of (11) are the same, but with variables for the network replaced accordingly by the variables for the solvent. Finally, the last row of (11) is approximated at  $(x_{i,j}, y_{i,j})$  by

$$\begin{aligned}
 & \frac{-\bar{\theta}_{i+\frac{1}{2},j}^n u_{i+\frac{1}{2},j}^n + \bar{\theta}_{i-\frac{1}{2},j}^n u_{i-\frac{1}{2},j}^n}{h} + \frac{-\bar{\theta}_{i,j+\frac{1}{2}}^n v_{i,j+\frac{1}{2}}^n + \bar{\theta}_{i,j-\frac{1}{2}}^n v_{i,j-\frac{1}{2}}^n}{h} + \\
 & \frac{-\bar{\theta}_{i+\frac{1}{2},j}^s u_{i+\frac{1}{2},j}^s + \bar{\theta}_{i-\frac{1}{2},j}^s u_{i-\frac{1}{2},j}^s}{h} + \frac{-\bar{\theta}_{i,j+\frac{1}{2}}^s v_{i,j+\frac{1}{2}}^s + \bar{\theta}_{i,j-\frac{1}{2}}^s v_{i,j-\frac{1}{2}}^s}{h} = 0
 \end{aligned} \tag{14}$$

Where necessary, we use second-order extrapolation to account for the no-slip boundary conditions.

For a grid with  $N$  cell-centers in the  $x$ -direction and  $M$  cell-centers in the  $y$ -direction, the above approximations can be collected in a  $(5NM - 2(N + M))$ -by- $(5NM - 2(N + M))$  linear system, which we denote by

$$\underbrace{\begin{bmatrix} \mathcal{L}_n^h - \mathcal{C}^h & \mathcal{C}^h & -\mathcal{G}_n^h \\ \mathcal{C}^h & \mathcal{L}_s^h - \mathcal{C}^h & -\mathcal{G}_s^h \\ \mathcal{G}_n^{hT} & \mathcal{G}_s^{hT} & 0 \end{bmatrix}}_{\mathcal{A}^h} \begin{bmatrix} \mathbf{u}^n \\ \mathbf{u}^s \\ p \end{bmatrix} = \begin{bmatrix} \nabla^h \Psi(\theta^n) \\ 0 \\ 0 \end{bmatrix} \quad (15)$$

This forms the discrete approximation to (11). Since we assume  $0 < \theta^n < 1$ , it follows, for example, from [26, Theorem 3.6] that the eigenvalues of  $\mathcal{A}^h$  have nonpositive real part ( $\mathcal{A}^h$  is negative semistable), i.e.  $\text{Re}(\lambda) \leq 0$  for all  $\lambda \in \sigma(\mathcal{A}^h)$ . This can be advantageous for (preconditioned) Krylov subspace methods [26].

For the temporal discretization of (9), we use explicit first order upwinding for the advective term  $\nabla \cdot (\theta^n \mathbf{u}^n)$  (specifically we use LeVeque's first order upwind with transverse wave corrections [27]), and we treat the diffusion implicitly with backward Euler. The linear system that arises because of the implicit discretization is solved using preconditioned GMRES solver in PETSc with block Jacobi as the preconditioner. For efficiency and stability, we use the adaptive time-stepping procedure described in [15].

The basic strategy we use for simulating the two-dimensional gel is as follows:

1. For a given  $\theta^n$  at time  $t$ , solve the discrete system (15) for  $\mathbf{u}^n$ ,  $\mathbf{u}^s$ , and  $p$  at time  $t$ .
2. Solve for  $\theta^n$  (and thus  $\theta^s$ ) at time  $t + \Delta t$  using upwinding for (9), as discussed in the previous paragraph, with the value of  $\mathbf{u}^n$  at time  $t$ .
3. Repeat step 1, with the  $\theta^n$  at  $t + \Delta t$ .

#### 4. SOLVING THE COUPLED MOMENTUM AND CONTINUITY EQUATIONS

To solve the discrete system (15), we use a collective (box) relaxation scheme within a multigrid procedure [17]. The box relaxation scheme updates unknowns locally, cell-by-cell, by solving a succession of small linear systems. The updated unknowns are used in a Gauss-Seidel manner as soon as they are available. The key elements of the algorithm are described below.

##### 4.1. Smoother

For the 2-D system (11) on the MAC grid, the box relaxation involves solving the discrete equations (15) locally in each computational cell (or box). For each interior box, this requires solving a 9-by-9 linear system (4 equations for the network velocity, 4 equations for the solvent velocity, and 1 equation for the pressure) for corrections to the unknowns  $\mathbf{u}^n$ ,  $\mathbf{u}^s$ , and  $p$ . With Dirichlet boundary conditions, boxes at the corners of the domain require solving 5-by-5 linear systems, while boxes on the edges require solving 7-by-7 systems. We update corrections to the unknowns in a Gauss-Seidel-type manner and combine this with underrelaxation with  $\omega = 0.675$ . Suppose the linear system on a single box is  $L\mathbf{x} = \mathbf{b}$ , where  $L$ ,  $\mathbf{x}$  and  $\mathbf{b}$  are the coefficient matrix, unknown vector and right hand side, respectively. Then after the  $(k + 1)$ th box relaxation:



$$\mathbf{x}^{k+1} = (1 - \omega)\mathbf{x}^k + \omega L^{-1}\mathbf{b} \quad (16)$$

The boxes are processed using red-black ordering. Note that vector values located at cell edges are relaxed twice while scalar values located at cell centers are relaxed once within each iteration. Parallelization similar to [18] is developed using the Message Passing Interface (MPI) for communication on distributed memory computers.

The parallel box relaxation works as follows. Suppose we have a portion of our two dimensional staggered grid on a specific processor as in Figure 3, with one layer of buffer cells. The solid thick line is the parallel subdomain boundary.

At the beginning of the sweep, the values stored in the buffer cells are current. Let  $(i, j)$  be the global cell index, then cells with  $(i + j) \bmod 2 = \text{even}$  are marked as red and those with  $(i + j) \bmod 2 = \text{odd}$  are marked as black. During the red sweep, the red cells in the subdomain are updated in lexicographic order. The updated velocity components (small rectangles) and pressures (circles) are shown in Figure 3(a). The red cells within the buffer are also simultaneously relaxed on neighboring processors but their state values are not yet available to this processor. After the red sweep, a two-stage communication process is carried out with adjacent processors to update the buffer states. The first stage exchanges local state values along the left and right subdomain boundaries with the corresponding neighboring processors. The updated states after the communication are cross-hatched in Figure 3(b). In order to distinguish the red and black relaxations, the states updated by the red sweep are indicated above or to the right of the cell edges and those updated by the black sweep are shown below or to the left of the edges. Updating the states in the upper and lower buffers is achieved through a similar communication step. Note that unlike the left-right communication, states on the corner cells such as those within the dashed circles in Figure 3(c) are also sent/received in order to interpolate corrections to the next finer grid for the subdomain. Explicit communications with diagonal neighbors are avoided since all the corner states have already been updated in the left-right communication step of the upper/lower processors. The black box relaxation is done in the same way, as shown in Figure 3(d-f). It is clear that after the final communication step, all velocity components have been relaxed twice and pressure components have been relaxed once. It is also clear that all buffer cells hold updated information and so the information to carry out another smoothing sweep is in place. Note also that the current values of all variables needed to compute residuals at subdomain cells are available at the end of each sweep.

#### 4.2. Transfer operators

Suppose the mesh-spacing in both the  $x$  and  $y$  directions is given by  $h$ , with  $1/h$  a power of 2. We define a sequence of coarser grids, where each grid is a factor of two coarser than the previous in both the  $x$  and  $y$  direction. After one iteration of box-relaxation, residuals  $r^h$  are calculated at the same locations on the MAC grid as the corresponding unknowns, and the right hand sides  $f^{2h}$  of the defect equations on the next coarser grid are formed through restriction with standard full-weighting. As shown in Figure 4(a), scalar quantities  $f^{2h}$  (pressure or volume fraction) at a coarse grid center  $F$  are calculated as the arithmetic average of the related  $r^h$  values at the fine grid centers 1, 2, 3 and 4. Six-point weighting is

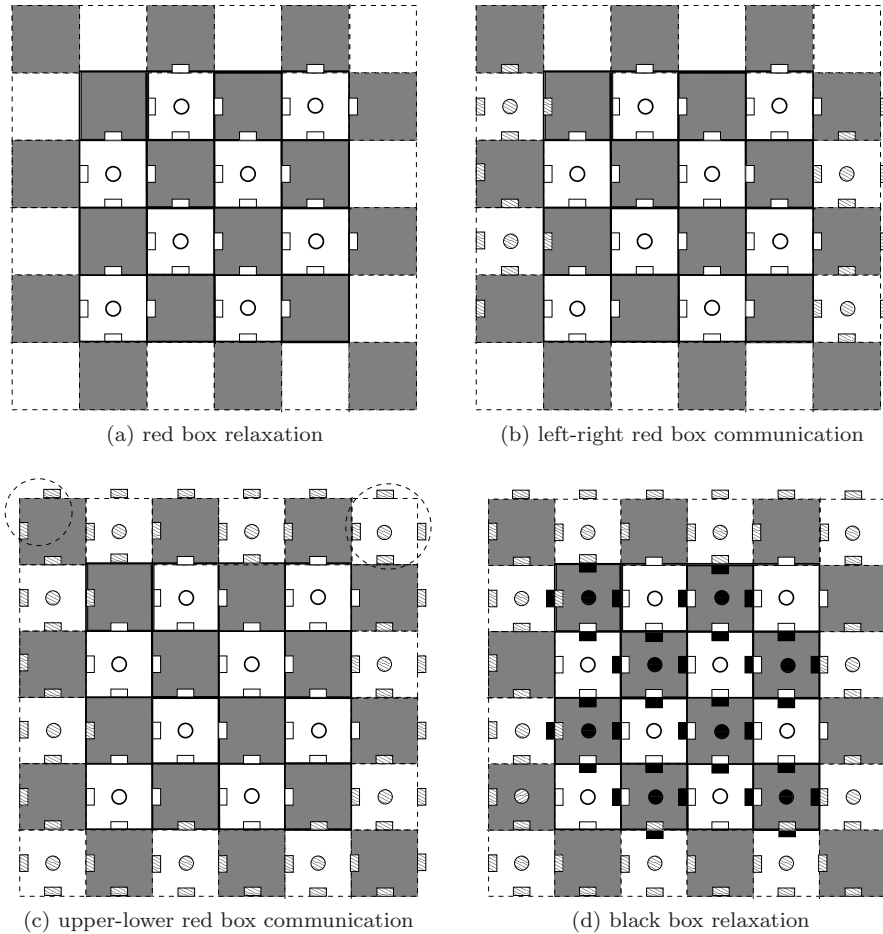


Figure 3: Progression of red-black Gauss-Seidel box-relaxation smoothing sweep. (a) After completion of the the red sweep, pressures at red cell centers and all velocities on red cell edges have been updated. (b) Updated red cell values are communicated to neighboring processors to the right and left to update red cell values in subdomain buffer cells. (c) Updated red cell values are communicated to neighboring processors above and below to update red cell values in subdomain buffer cells. (d) After completion of the black sweep, pressures at black cell centers and all velocities on black cell edges have been updated. (e) Updated black cell values are communicated to neighboring processors to the right and left to update black cell values in subdomain buffer cells. (f) Updated black cell values are communicated to neighboring processors above and below to update black cell values in subdomain buffer cells.

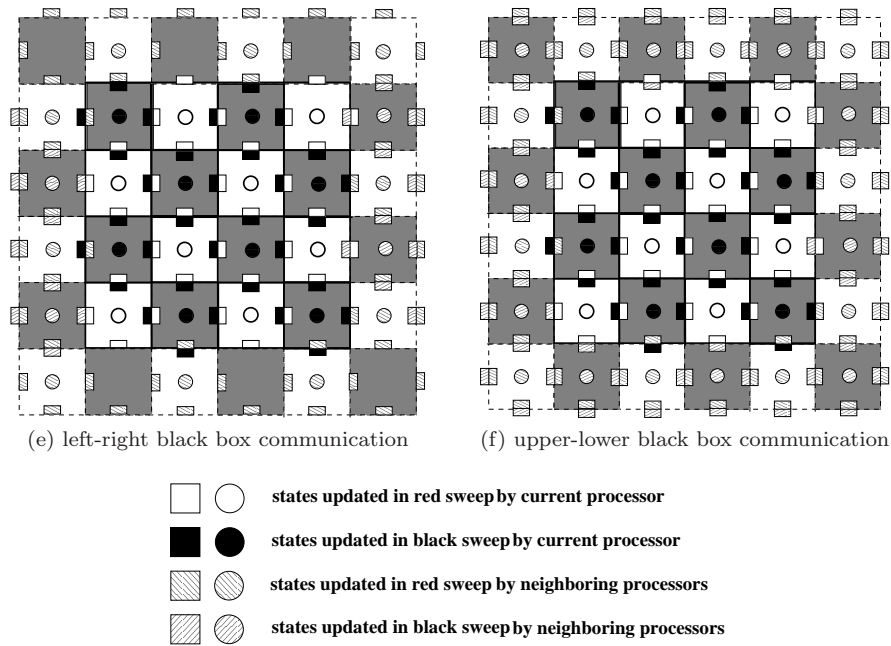


Figure 3: Continued

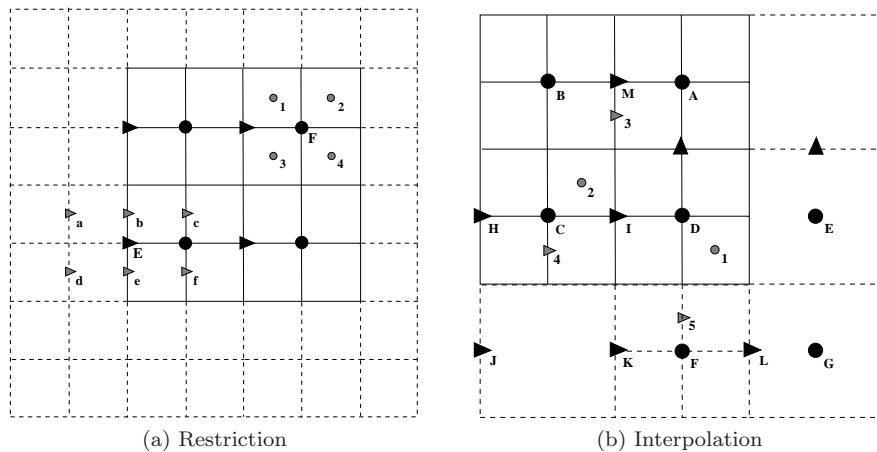


Figure 4: Multigrid transfer operators: (a) Restriction: For variables at cell centers (F), restriction is the arithmetic average of values from the neighboring fine grid points (1,2,3,4). For variables at cell edges (E), restriction uses a weighted average of values at the neighboring edges (a-f). (b) Interpolation: The value of a variable at a fine grid cell center (2) is calculated by bilinear interpolation from neighboring course grid cell centers (A, B, C, D). The value of variables at fine grid cell edges such as points 3 or 4 are interpolated by linear interpolation from the neighboring two (I and M) coarse grid cell edges or by bilinear interpolation from the four neighboring coarse grid cell edges (H, I, J, K).

used for vector values at a coarse grid edge center  $E$ :

$$f^{2h}(F) = \frac{1}{4}[r^h(1) + r^h(2) + r^h(3) + r^h(4)] \quad (17)$$

$$f^{2h}(E) = \frac{1}{8}[r^h(a) + r^h(c) + r^h(d) + r^h(f) + 2r^h(b) + 2r^h(e)] \quad (18)$$

Note that communication is needed to provide current fine grid residual values with the fine grid buffers (dashed cells) such as at points  $a$  and  $d$ , before the restriction is carried out.

After reaching the coarsest grid, corrections on the next finer grid are calculated by linear/bilinear interpolation and box relaxation is carried out again with the corrected state values. In Figure 4(b), point 2 is a fine grid center, and points 3 and 4 are centers of fine grid cell edges. The corrections for the pressure ( $Cp_h$ ) and the velocity ( $Cv_h$ ) are calculated from the related coarse grid values as:

$$Cp_h(2) = \frac{1}{16}[9P_{2h}(C) + 3P_{2h}(B) + 3P_{2h}(D) + P_{2h}(A)] \quad (19)$$

$$Cv_h(3) = \frac{1}{4}[3V_{2h}(M) + V_{2h}(I)] \quad (20)$$

$$Cv_h(4) = \frac{1}{8}[3V_{2h}(H) + 3V_{2h}(I) + V_{2h}(J) + V_{2h}(K)] \quad (21)$$

where  $P_{2h}$  and  $V_{2h}$  are the pressure and the velocity on coarse grid. Note that it is also necessary to interpolate corrections to those fine grid points in the buffer (e.g., point 5) which is within the processor's subdomain on the finer grid. Obviously, buffer state values at points such as  $E$ ,  $F$ ,  $G$  and  $J$ ,  $K$ ,  $L$  are needed to interpolate corrections at points 1, 4 and 5. Since these values are already available through the communication step of box relaxation, no additional communications are required for interpolation.

#### 4.3. Parallel multigrid on coarsest grid

The relative communication overhead increases as the grid gets coarser during the multigrid cycle, and it is known that this may result in a significant loss of efficiency for the parallel application. We use the agglomeration method to overcome the problem. Specifically, in our implementation, if the grid is coarse enough so that there is only one grid cell in the  $x$  or  $y$  direction for any of the processors, data values (right hand side and volume fraction) are gathered and distributed globally onto every processor through an all-to-all communication procedure. Then each processor solves the same system of equations on the entire coarsest grid using Gaussian elimination with pivoting, and updates the data within its own subdomain. Since the size of the system to solve grows with the number of processors, the box relaxation scheme mentioned before with a prescribed small number of iterations (e.g. 5 for the simulation results presented here) is employed instead of the direct method in cases when the latter becomes too expensive. Therefore, the parallel multigrid algorithm, in which the coarsest grid level depends on the number of processors, and in which the coarsest grid equations are solved approximately, is different from its serial counterpart, in which the coarsest possible grid is used and the coarsest grid equations are solved exactly. As a result, the numerical efficiency may be reduced although the above strategies may increase the parallel efficiency. It is the balance between the two that should be optimized [28].

#### 4.4. Multigrid as preconditioner for GMRES

It is shown in [15] that multigrid used on its own as the solver for the gel system may not be very robust, especially when phase separation occurs. The reason is the appearance of a few large isolated eigenvalues of the multigrid iteration matrix. It is also shown in [15] that these large eigenvalues are well captured by a Krylov acceleration technique [29]. Specifically, the multigrid procedure just described is used as a (right) preconditioner for GMRES solution of the system (15). The multigrid-preconditioned GMRES procedure is robust and efficient even when sharp gradients in volume fraction develop during the gel separation process. We follow the same strategy for the parallel algorithm by using the multigrid box relaxation scheme as a preconditioner for the parallel GMRES solver in PETSc [24]. The Krylov method is applicable to non-symmetric matrices and non-positive definite preconditioners, both of which are found for the gel system. One multigrid sweep is carried out per Krylov iteration.

If we let  $y^T = [(u^n)^T \ (u^s)^T \ p^T]$  and  $f$  be the right hand side of (15), the preconditioned system of equations to solve with GMRES is given by

$$\mathcal{A}^h(\mathcal{M}^h)^{-1}z = f \quad (22)$$

where  $z = \mathcal{M}^h y$ , and  $\mathcal{M}^h$  represents the preconditioning matrix from the multigrid box relaxation scheme. As shown in [30], the  $(m+1)$ th iteration of the multigrid procedure can be written in the form

$$y^{(m+1)} = (I - (\mathcal{M}^h)^{-1}\mathcal{A}^h)y^{(m)} + (\mathcal{M}^h)^{-1}f \quad (23)$$

Applying this once with zero initial guess gives

$$y^{(1)} = (\mathcal{M}^h)^{-1}f$$

This is exactly what we do when applying multigrid once as a preconditioning matrix to vector  $f$ . Therefore the multigrid preconditioner always takes zero as the initial guess, the input vector as the right hand side, and sets the updated state variables after one multigrid iteration to be the output vector. Function `PCShellSetApply(pc, (*apply)(void*, Vec, Vec))` in PETSc provides a convenient way to implement a user-defined parallel preconditioner, where `pc` is the preconditioner context and `apply` is the user-provided preconditioning routine. The first input argument `apply` is a void pointer and can be cast to whatever the user has set the application-defined context to be and the other two arguments are global input and output vectors [24].

We consider the system (15) at time  $t$  “solved” when the residual of the  $\ell^{\text{th}}$  iterate of the respective method satisfies

$$\frac{\|r^{(\ell)}\|_2}{\|f\|_2} \leq 10^{-6} \quad (24)$$

where  $\tilde{r}^{(\ell)} = f - \mathcal{A}^h y^{(\ell)}$ . Unless otherwise specified, for all time steps but the initial one, we use the previous time step’s values for the network and solvent velocities and pressure as initial guesses for the iterative methods. After solving system (15), updated values of the network velocity are communicated to the appropriate buffer cells. These values are needed at the beginning of the next time step in order to evaluate the discrete advection terms in approximating the continuity equation (9) for  $\theta^n$ .

## 5. NUMERICAL RESULTS

To test the method in 2-D, we let the domain be the unit square and start with an initial distribution of network  $\theta^n$  that is perturbed about the unstable region of the osmotic pressure  $\Psi$  (cf. Figure 1):

$$\theta^n = 0.08 + 2.5 \cdot 10^{-4}(\cos(6\pi x) + \cos(4\pi y))$$

The model parameters are set to  $\mu_n = 0.1$ ,  $\lambda_n = 0.3$ ,  $\mu_s = 0.025$ ,  $\lambda_s = 0$ ,  $\beta = 1$ , and  $\kappa = 10^{-7}$ . The first four of these values make  $\alpha_n = 0.5$  and  $\alpha_s = 0.05$ . Note that multigrid F-cycle is always used for cycling through the grids. Plots of the network volume fraction and velocity field at various stages of gel phase separation are shown in Figure 6. Figure 5 shows the network volume fraction  $\theta^n$  distributions along  $x = 0.5$  for different time steps. Clearly as time evolves, the network and solvent phases separate and channels with sharp edges form. The simulation was run on 16 processors with a  $512 \times 512$  grid, using multigrid preconditioned GMRES as the solver for the momentum equations.

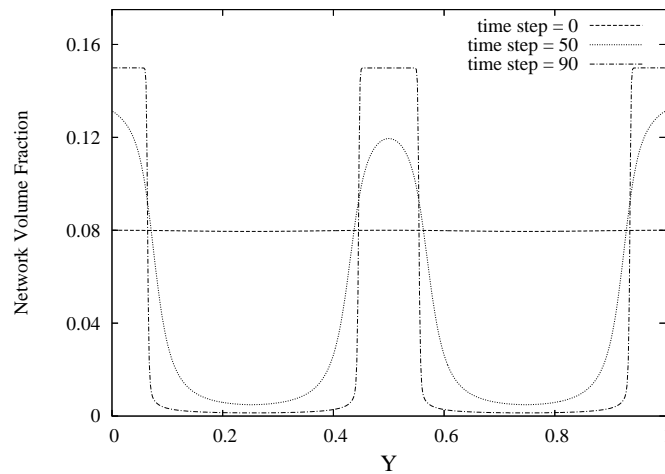
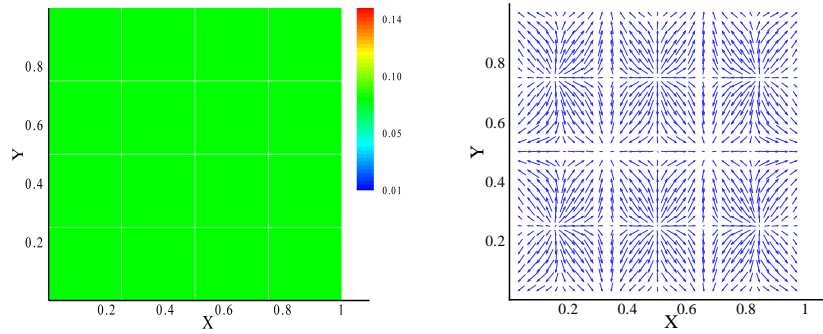
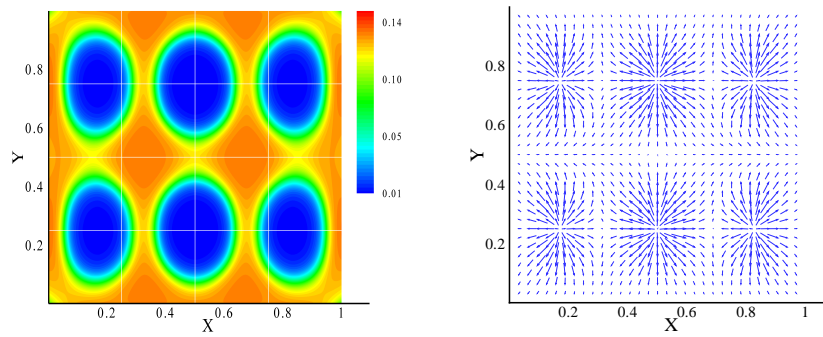


Figure 5: Network volume fraction distribution along  $x = 0.5$  at different time steps.

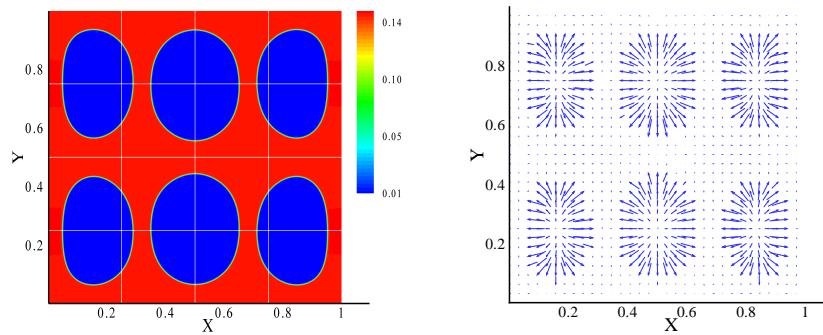
Figures 7 and 8 display the number of iterations needed to satisfy the relative residual condition (24) for multigrid (F-cycle) as a stand-alone solver (MGF) and as preconditioner for GMRES (GMRES-MGF) with mesh size  $512 \times 512$  at different time steps during the simulation. The results are for serial ( $1 \times 1$ ) and parallel simulations with 32 processors ( $8 \times 4$  parallel decomposition). As pointed out in [18], since cells of the same color are still coupled with each other, a degradation in the smoothing rate of the scheme may be expected as the number of processors increases. Another source for the degradation may be the reduction in the number of multigrid levels as the number of processors increases, along with the approximate iterative solution of the coarsest grid equations (see Section 4.3). It is clear from the figures that this degradation, increasing the number of iterations by 1 – 3, is not severe with a moderate number of processors. By comparing with Figure 5, it can be seen that the number of iterations required by the numerical solvers remains approximately constant until channels with sharp



Step = 1, Time = 39.70,  $V_{max} = 1.51e-05$



Step = 50, Time = 153.87,  $V_{max} = 3.69e-3$



Step = 110, Time = 401.59,  $V_{max} = 1.76e-4$

Figure 6: Network volume fraction (left) and distribution of the network velocity (right).  $V_{max}$  is the largest velocity value in the plot.

edges form. Starting at this stage, the number of iterations for MGF increases sharply. In fact, MGF fails to converge in the later stages of gel separation within 30 iterations. In contrast, GMRES-MGF performs well for all stages of gel separation, showing only a moderate increase of iterations. Therefore, as previously mentioned in [15], using multigrid as the preconditioner for GMRES yields a more robust solver than multigrid alone.

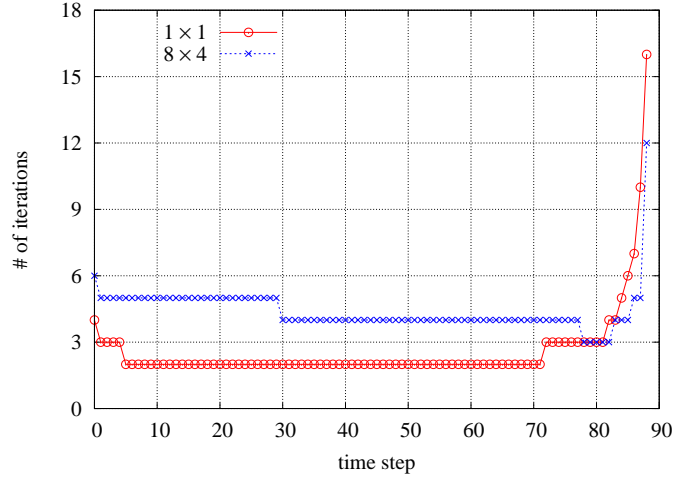


Figure 7: Number of iterations for MGF at different time steps for 1 and 32 processors.

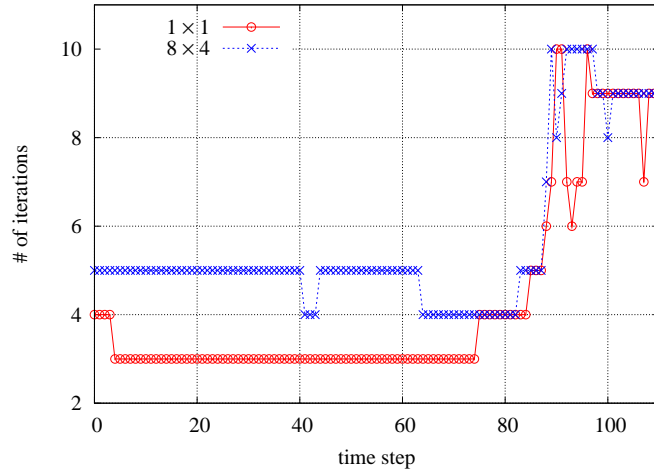


Figure 8: Number of iterations for GMRES-MGF at different time steps for 1 and 32 processors.

By choosing a time step in which the serial and parallel methods required the same number of iterations, the speedup of the code within one time step of a simulation was determined. This



is plotted in Figure 9 for grid sizes of  $1024 \times 1024$  and  $512 \times 512$ . It is clear that for a sufficiently large problem, the code shows good scalability. Table I shows the detailed information about the wall clock time distribution percentage for parallel runnings with different number of processors. The results for the last column include parallel box relaxation, residual evaluation and intergrid transfers, which are fully parallelizable. Smoothing on coarsest grid only makes use of one processor and forms the serial part of the algorithm.

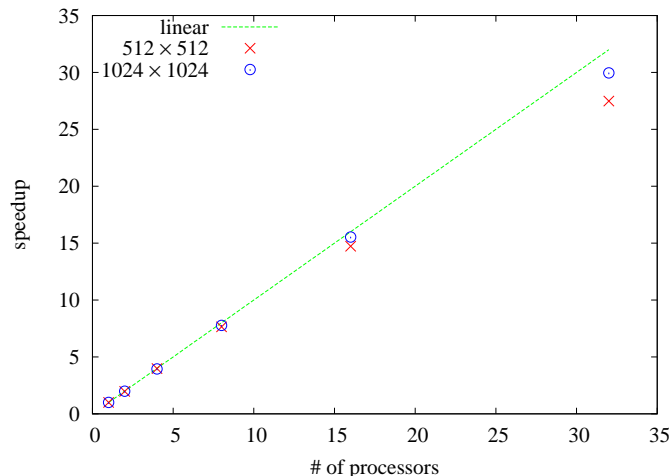


Figure 9: Speedup plot for GMRES-MGF for different sized grids.

## 6. CONCLUSIONS

We have presented a computational methodology for simulating models of two-phase gel dynamics. The main computational challenge of these models is in solving the momentum and incompressibility equations which involve variable-coefficient differential terms and terms coupling the two fluids. Our method of solving this system by using parallel multigrid with a box-type relaxation procedure as a preconditioner for GMRES solver in PETSc package appears to be very effective with good parallel performance. Numerical results from model problems in two dimensions indicate the method is both robust and efficient.

## ACKNOWLEDGEMENT

This work was supported in part by NSF grant DMS-0540779. We gratefully acknowledge a grant of computing time from the Center for High Performance Computing at the University of Utah.

## REFERENCES

1. Alt W, Dembo M. Cytoplasm dynamics and cell motion: two-phase flow models. *Mathematical Biosciences* 1999; **156**:207-228.
2. Cogan NG, Keener JP. Channel formation in gels. *SIAM Journal on Applied Mathematics* 2005; **65**:1839-1854.
3. Dembo M. Mechanics and control of the cytoskeleton in Amoeba proteus. *Biophysical Journal* 1989; **55**(6):1053-1080.
4. Dembo M, Harlow F. Cell motion, contractile networks, and the physics of interpenetrating reactive flow. *Biophysical Journal* 1986; **50**(1):109-121.
5. Doi M, Onuki A. Dynamic coupling between stress and composition in polymer solutions and blends. *Journal de Physique II France* 1992; **2**:1631-1656.
6. He XY, Dembo M. On the mechanics of the first cleavage division of the sea urchin egg. *Experimental Cell Research* 1997; **233**(2):252-273.
7. Tanaka H. Viscoelastic phase separation. *Journal of Physics: Condensed Matter* 2000; **12**:R207-R264.
8. Drew DA. Mathematical modeling of two-phase flow. *Annual Review of Fluid Mechanics* 1983; **15**:261-291.
9. Drew DA, Passman SL. Theory of multicomponent fluids. In *Applied Mathematical Sciences*, Marsden JE, Sirovich L. (ed.). Springer: New York, 1999.
10. Lemon G, King JR, Byrne HM, Jensen OE, Shakesheff KM. Mathematical modelling of engineered tissue growth using a multiphase porous flow mixture theory. *Journal of Mathematical Biology* 2006; **52**(5):571-594.
11. Byrne H, Preziosi L. Modelling solid tumour growth using the theory of mixtures. *Mathematical Medicine and Biology* 2003; **20**(4):341-366.
12. Lubkin SR, Jackson T. Multiphase mechanics of capsule formation in tumors. *Journal of Biomechanical Engineering* 2002; **124**(2):237-243.
13. Alpkvist E, Klapper I. A multidimensional multispecies continuum model for modelling biofilm development. *Bulletin of Mathematical Biology* 2007; **69**:765-789.
14. Cogan NG, Keener JP. The role of the biofilm matrix in structural development. *Mathematical Medicine and Biology* 2004; **21**:147-166.
15. Wright GB, Guy RD, Fogelson AL. An efficient and robust method for simulating two-phase gel dynamics. *SIAM Journal on Scientific Computing* 2008, to appear.
16. Harlow FH, Welch JE. Numerical calculation of time-dependent viscous incompressible flow of fluid with free surfaces. *Physics of Fluids* 1965; **8**:2182-2189.
17. Vanka SP. Block-implicit multigrid solution of Navier-Stokes equations in primitive variables. *Journal of Computational Physics* 1986; **65**:138-158.
18. Degani AT, Fox GC. Parallel multigrid computation of the unsteady incompressible Navier-Stokes equations. *Journal of Computational Physics* 1996; **128**(1):223-236.
19. Manservigi S. Numerical analysis of Vanka-type solvers for steady Stokes and Navier-Stokes flows. *SIAM Journal on Scientific Computing* 2006; **44**:2025-2056.
20. Sivaloganathan S. The use of local mode analysis in the design and comparison of multigrid methods. *Computer Physics Communications* 1991; **65**:246-252.
21. Thompson MC, Ferziger JH. An adaptive multigrid technique for the incompressible Navier-Stokes equations. *Journal of Computational Physics* 1989; **82**:94-121.
22. Trottenberg U, Oosterlee CW, Schüller A. *Multigrid*. Academic Press: London, 2000.
23. Wesseling P, Oosterlee CW. Geometric multigrid with applications to computational fluid dynamics. *Journal of Computational and Applied Mathematics* 2001; **128**:311-334.
24. Balay S, Gropp W, McInnes L, Smith B. PETSc Users Manual. *ANL-95/11*. Argonne National Laboratory, 2001.
25. Allen RD, Cowden RR. Syneresis in ameboid movement: Its localization by interference microscopy and its significance. *The Journal of Cell Biology* 1962; **12**:185-189.
26. Benzi M, Golub GH, Liesen J. Numerical solution of saddle point problems. *Acta Numerica* 2005; **14**:1-137.
27. Leveque RJ. High-resolution conservative algorithms for advection in incompressible flow. *SIAM Journal on Numerical Analysis* 1996; **33**:627-665.
28. John V. A comparison of parallel solvers for the incompressible Navier-Stokes equations. *Computing and Visualization in Science* 1999; **1**(4):193-200.
29. Oosterlee CW, Washio T. An evaluation of parallel multigrid as a solver and a preconditioner for singularly perturbed problems. *SIAM Journal on Scientific Computing* 1998; **19**:87-110.
30. Saad Y. *Iterative Methods for Sparse Linear Systems*. SIAM: Philadelphia, 2003.

# of processors	Communication	Smoothing on coarsest grid	Others
8	2.7%	0.8%	96.5%
16	6.8%	2.3%	90.9%
32	11.1%	5.1%	83.8%

Table I: Wall clock time distributions for simulations on  $1024 \times 1024$  grid.